

$$w = \int P \, dv \quad \text{Quasi-equilibrium (reversible) process;}$$

$$h = u + Pv \quad \text{Definition, always true}$$

$$PV = mRT = n\bar{R}T \quad \text{Ideal gas (T > 2*T_{crit}, P < 10 MPa)}$$

$$\begin{aligned} u &\approx u_f @ T; \quad v \approx v_f @ T \quad \text{Subcooled liquid} \\ h &\approx h_f @ T + v_f(P - P_{sat}) \quad \text{Subcooled liquid} \\ v &= v_f + x(v_g - v_f), \quad u = u_f + x u_{fg} \quad \text{Two-phase} \end{aligned}$$

$$Q - W = E_2 - E_1 \quad \text{First law for a process, no constraints}$$

$$Q - W = U_2 - U_1 \quad \text{First law for a process, closed system, negligible changes in kinetic and potential energy}$$

$$C_v = \frac{\partial u}{\partial T}, \quad C_p = \frac{\partial h}{\partial T} \quad \text{Definition;}$$

$$C_v = \frac{du}{dT}, \quad C_p = \frac{dh}{dT} \quad u \text{ and } h \text{ functions of temperature only}$$

$$u_2 - u_1 = \int C_v \, dT \quad \text{Internal energy is a function of temp only; } h_2 - h_1 = \int C_p \, dT \quad \text{Enthalpy is a function of temp only}$$

$$\oint \delta Q = \oint \delta W \quad \text{Any thermodynamic cycle}$$

$$\dot{m} = \rho \vec{V} A \quad \text{steady, 1-d flow}$$

$$\dot{Q} + \sum \dot{m}_i(h + \frac{\vec{V}^2}{2} + gZ)_i = \dot{W} + \sum \dot{m}_e(h + \frac{\vec{V}^2}{2} + gZ)_e + \frac{dE}{dt} \quad \text{First law for control volume}$$

$$q + h_1 + \frac{1}{2}\vec{V}_1^2 + gZ_1 = w + h_2 + \frac{1}{2}\vec{V}_2^2 + gZ_2 \quad \text{Single-inlet, single-exit, steady flow}$$

$$\eta_{th} = \frac{W_{net}}{q_H} = 1 - \frac{q_L}{q_H} \quad \text{Heat engine; } \beta = \frac{q_L}{W_{net}} \quad \text{Heat pump (cooler); } \gamma = \frac{q_H}{W_{net}} \quad \text{Heat pump (heater)}$$

$$w = - \int v \, dP - \frac{1}{2}(\vec{V}_2^2 - \vec{V}_1^2) - g(Z_2 - Z_1) \quad \text{Reversible, steady flow}$$

$$q = \int T ds \quad \text{Reversible process}$$

$$Q_H/Q_L = T_H/T_L \quad \text{Carnot cycle}$$

$$\frac{T_2}{T_1} = \left(\frac{P_2}{P_1} \right)^{\frac{k-1}{k}}; \quad \frac{T_2}{T_1} = \left(\frac{v_2}{v_1} \right)^{1-k}; \quad \frac{P_2}{P_1} = \left(\frac{v_1}{v_2} \right)^k \quad s = \text{const, IG, Cp = const}$$

$$\Delta s = C_p \ln \frac{T_2}{T_1} - R \ln \frac{P_2}{P_1}, \quad \Delta s = C_v \ln \frac{T_2}{T_1} + R \ln \frac{v_2}{v_1} \quad \text{IG, const specific heats}$$

$$\frac{P_{R2}}{P_{R1}} = \frac{P_2}{P_1}; \quad \frac{v_{R2}}{v_{R1}} = \frac{v_2}{v_1} \quad \text{Isentropic, ideal gas, non-constant specific heats}$$

$$\eta_{turbine} = w_a/w_s \quad \eta_{compressor} = w_s/w_a \quad \eta_{pump} = w_s/w_a \quad \eta_{nozzle} = \frac{\vec{V}_a^2}{\vec{V}_s^2}$$



